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² Conservative, bounded, and nonlinear discretization of the ³ Cahn-Hilliard-Navier-Stokes equations

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A B S T R A C T

The Cahn-Hilliard equation describes phase separation in a binary mixture, typically modeled with a phase variable that represents the concentration of one phase or the concentration difference between the two phases. Though the system is energetically driven toward solutions within the physically meaningful range of the phase variable, numerical methods often struggle to maintain these bounds, leading to physically invalid quantities and numerical difficulties. In this work, we introduce a novel splitting and discretization for the Cahn-Hilliard equation, coupled with the Navier-Stokes equations, which inherently preserves the bounds of the phase variable. This approach transforms the fourth-order Cahn-Hilliard equation into a second-order Helmholtz equation and a second-order nonlinear equation with implicit energy barriers, which is reformulated and solved with a safeguarded optimization-based solution method. Our scheme ensures the phase variable remains in the valid range, robustly handles large density ratios, conserves mass and momentum, maintains consistency between these quantities, and achieves second-order accuracy. We demonstrate the method's effectiveness through a variety of studies of two-dimensional, two-phase fluid mixtures.

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11 1. Introduction

¹² The Cahn-Hilliard equation describes the separation of a binary fluid mixture into domains that are pure in each ¹³ phase [10, 20]. The mixture is typically modeled with a phase variable γ that represents the concentration of one phase ¹⁴ (γ ∈ [0, 1]) or the concentration difference between the two phases (γ ∈ [-1, 1]). A variety of schemes have been ¹⁵ developed for the numerical solution of the Cahn-Hilliard equation, including Fourier spectral methods [55, 32, 41], 16 finite difference methods [26, 43, 30, 12, 36], and finite element methods [21, 9, 7, 24, 52, 31]. Though the system is

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17 energetically driven toward solutions within the physically meaningful range of γ , numerical methods for the solution of the Cahn-Hilliard equation may generate values outside this range, leading to physically invalid quantities and numerical difficulties [27, 35, 37]. Specifically, the phase variable is used to compute effective densities and viscosi-²⁰ ties. Under large density ratios, even a small excursion outside the valid range of values for γ can result in negative ²¹ effective densities, and hence ill-posedness of the viscous momentum equation and loss of positive-definiteness in numerical solvers.

₂₃ To model two-phase incompressible flows, the Cahn-Hilliard equation is coupled to the incompressible Navier- $_{24}$ Stokes equations. Several works have investigated variants of this system, including the case of matched densities [33, 4], the Boussinesq approximation [38, 45, 3], and the more general Cahn-Hilliard-Navier-Stokes (CHNS) equations 26 with varying densities and viscosities $[51, 50, 40, 16, 19, 30, 36, 27]$.

 Cahn-Hilliard models vary based on the choice of potential and mobility functions, and this impacts the theoret- ical boundedness properties of the phase variable. A common approach is to use the Ginzburg-Landau double-well polynomial potential with constant mobility [25, 36, 27], suitable for situations where the diffusion is not strongly dependent on the concentration field. This model permits the phase variable to go outside physically meaningful 31 bounds. The Cahn-Hilliard model with concentration-dependent degenerate mobility, which is zero in pure phases, has also been widely used [7]. In this form, given initial data that satisfies the physical bounds, the solution has been shown to maintain the bounds [22]. Another commonly employed model uses a logarithmic potential based on the Flory-Huggins theory of polymer solutions [1, 11, 5]. The potential is singular with infinite energy barriers at the pure 35 concentrations $\gamma = 0$ or $\gamma = 1$, preventing the solution from attaining or exceeding these values. This formulation ³⁶ admits a maximum principle so that the analytic solution remains within bounds [15, 47, 1].

³⁷ Preserving the physical bounds of the phase variable in numerical solutions can be challenging even in models that admit a maximum principle. This requirement may also impose additional time step restrictions [14, 6, 48]. There have been many works aimed at developing bounds-preserving numerical methods. Several methods have addressed 40 the issue of keeping γ in its physical bounds by using combinations of flux and slope limiters [25, 44]. Another approach to maintain the bounds of the phase variable is to explicitly clamp the variable in regions that exceed the bounds [18]. However, in order to conserve mass, the clipped mass must then be redistributed in a bounds-respecting manner. Chiu and Lin [13] applied such a strategy, uniformly distributing the clipped mass in the interfacial transition region. Huang et al. [35] proposed a boundedness mapping, a volume redistribution scheme that maintains the phase variable in the physical range. This method determines a set of conservative fluxes that maintain the global mass of the system while distributing mass from regions that undershoot or overshoot. This method was used to maintain bounds in the simulation of the Cahn-Hilliard-Navier-Stokes equations in both [36] and [27]. One drawback of the approach ⁴⁸ is that the choice of mass redistribution is controlled by a weight function and the determination of the fluxes requires a computationally expensive Poisson equation solve. The boundedness mapping approach was further developed in [37] for the more challenging case of multiphase flows with three or more phases.

 When modeled with a singular logarithmic potential, numerical methods for the Cahn-Hilliard equation must be carefully designed to maintain the solution strictly within the physical bounds. Copetti and Elliott [14] developed a

 piecewise linear finite element scheme with backward Euler time discretization for the Cahn-Hilliard equation with a logarithmic free energy and gave conditions on the time step and initial data to ensure boundedness of the solution. Barrett and Blowey [6] further proved error bounds for this scheme. Yang and Zhao [53] developed an unconditionally energy-stable scheme for the CH equation with logarithmic potential that is linear and symmetric positive definite.

⁵⁷ Based on the work of Eyre [23], several approaches utilize convex splitting, where the potential is expressed as ⁵⁸ a difference of convex functions and a convex nonlinear subproblem is formulated and solved implicitly to maintain ⁵⁹ the solution bounds. Li et al. [42] proposed an unconditionally stable nonlinear scheme based on convex splitting of ⁶⁰ the potential and solved by Newton iteration. The convergence of the scheme was analyzed in [17] by converting the ⁶¹ problem into a convex minimization. Also based on a convex splitting of the potential and implicit treatment of the ⁶² logarithmic terms, Chen et al. [11] developed first and second order finite difference schemes where the positivity of ⁶³ the logarithmic argument is maintained without incurring an additional time step restriction.

⁶⁴ Bailo et al. [5] used a convex splitting approach combined with an upwind methodology for discretization of the ⁶⁵ mobility to construct a semi-implicit scheme that unconditionally maintains the boundedness of the phase variable. ⁶⁶ Acosta-Soba et al. [2] also pursued an upwind methodology for both the flow velocity and the mobility in a discontin-⁶⁷ uous Galerkin scheme for the convective Cahn-Hilliard equation with polynomial potential and degenerate mobility, ⁶⁸ maintaining the bounds on the solution. A bounds-preserving upwind scheme was also developed in [34].

⁶⁹ In this work, we introduce a novel splitting for the numerical solution of the Cahn-Hilliard-Navier-Stokes equa-⁷⁰ tions that maintains the phase variable $\gamma \in [0, 1]$ by construction. We use a piecewise potential approximation with 71 logarithmic terms singular at the pure phases. Similar to convex splitting approaches, our method results in a nonlin- 72 ear equation implicit in the phase variable that maintains boundedness of the solution. We reformulate the nonlinear ⁷³ equation as a convex optimization facilitating solution through a safeguarded optimization-based scheme. Existing ⁷⁴ approaches enforce the bounds constraint on γ by using a barrier energy, preventing γ from leaving the feasible region ⁷⁵ by requiring infinite energy to do so. Barriers of this type lead to poorly-conditioned numerical problems. We instead ⁷⁶ enforce the constraint $0 \le \gamma \le 1$ by construction, computing γ as the output of a function that cannot produce a value τ outside of the feasible range. Practically, this has the effect of moving our energy barrier energy out to infinity, result- 78 ing in an energy that grows slowly and is well-behaved everywhere. The resulting method is observed to be second ⁷⁹ order accurate and can robustly simulate large density ratios. We demonstrate the method's effectiveness through a ⁸⁰ variety of studies of two-dimensional, two-phase fluid mixtures.

81 2. Governing equations

⁸² *2.1. Cahn-Hilliard equation*

The Cahn-Hilliard equations can be expressed as

$$
\frac{\partial \gamma}{\partial t} + \nabla \cdot (\mathbf{u}\gamma) = \nabla \cdot (M\nabla \xi) + S_{\gamma}
$$
\n(1)

$$
\xi = \lambda (F'(\gamma) - \nabla^2 \gamma) \tag{2}
$$

$$
\lambda = \frac{3}{2\sqrt{2}}\sigma\eta.
$$
 (3)

Fig. 1: The MAC grid stores γ and pressure on cell centers (circles). Velocties are stored by component on faces (represented by triangles), (Reproduced from [27].)

83 We label the two fluid phases as 0 and 1. The volume fraction of fluid 1 is represented as the phase-field function $84 \gamma \in [0, 1]$. The chemical potential is ξ. λ, called the mixing energy density in Huang et al. [35], is a parameter that ⁸⁵ incorporates the surface tension constant σ and η , a parameter which influences the width of the phase transition ⁸⁶ region. **u** is the fluid velocity, *M* is the mobility, S_γ is an external source term, and *F* is a double well potential ϵ ⁸⁷ function. The details of *F* and its corresponding derivative *F'* are described in Section 3.1.2.

The properties of fluid phases 0 and 1 are density (ρ_0, ρ_1) and viscosity (μ_0, μ_1) respectively. For a given location x, we compute the effective density and viscosity of the phase mixture with

$$
\rho(\mathbf{x}) = \rho_0 + (\rho_1 - \rho_0) \gamma(\mathbf{x}) \tag{4}
$$

$$
\mu(\mathbf{x}) = \mu_0 + (\mu_1 - \mu_0) \gamma(\mathbf{x}).
$$
\n(5)

⁸⁸ *2.2. Navier-Stokes equations*

The Navier-Stokes equations for incompressible flow are given by

$$
\frac{\partial \rho}{\partial t} + \nabla \cdot \mathbf{m} = S_m \tag{6}
$$

$$
\nabla \cdot \mathbf{u} = 0 \tag{7}
$$

$$
\frac{\partial(\rho \mathbf{u})}{\partial t} + \nabla \cdot (\mathbf{m} \otimes \mathbf{u}) = -\nabla p + \nabla \cdot (\mu (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)) + \rho g + \sigma \kappa \nabla (h(\gamma)) + S_{\mathbf{u}},
$$
\n(8)

⁸⁹ where *ρ* is the effective density, **m** is the mass flux consistent with the γ evolution (1) [36], S_m is an external mass ⁹⁰ source, **u** is the velocity, *p* is the pressure, *μ* is the effective viscosity, *g* is the acceleration of gravity, *σ* is the coefficient 91 of surface tension, *κ* is the interface curvature, $h(y)$ is a regularized Heaviside function as defined in [27], and *S*_u is 92 the external momentum source.

93 3. Discretizations

⁹⁴ In this section we describe the temporal and spatial discretizations of the Cahn-Hilliard and Navier-Stokes equa-95 tions. As in [27], we use a uniform MAC grid (Figure 1) with γ and pressure stored at cell centers. Velocities are ⁹⁶ split by components and stored on cell faces. Unless otherwise specified, we use the same discretizations as in [27].

⁹⁷ *3.1. Cahn-Hilliard equation*

98 Goulding et al. [27] introduced a discretization that was simple and effective, but it did not ensure $\gamma \in [0, 1]$. ⁹⁹ Instead, they used the bounds-enforcing scheme introduced in Huang et al. [35] to correct gamma in a postprocess. ¹⁰⁰ That postprocess is non-local, which is undesirable since mass conservation is a local conservation property. It also ¹⁰¹ requires a Poisson solve to determine associated conservative fluxes which incurs significant computational cost [27]. 102 In this work, we construct a scheme that automatically guarantees $\gamma \in (0, 1)$ without the need for any postprocessing 103 steps. We do this by formulating *F* with a barrier at 0 and 1 (much as some existing formulations of *F* do [10]) and treating the term $F'(\gamma^{n+1})$ implicitly.

¹⁰⁵ *3.1.1. Scheme derivation*

We begin our formulation of our scheme with the scheme from [27] where the fourth order Cahn-Hilliard equation is split into two second-order Helmholtz equations as

$$
A - s\widehat{\Delta t}\nabla^2 A = \gamma^* + B + \widehat{\Delta t}S_{\gamma}^{n+1}
$$
\n(9)

$$
\gamma^{n+1} - s\widehat{\Delta t} \nabla^2 \gamma^{n+1} = A - B,\tag{10}
$$

γ

where γ^* is the result of advecting γ^n . In the absence of source terms, the scheme should be discretely mass conserving, requiring

$$
\int_{\Omega} \gamma^{n+1} \, dV = \int_{\Omega} \gamma^n \, dV \tag{11}
$$

Note that by the divergence theorem, any field *B* with zero flux or periodic boundary conditions satisfies

$$
\int_{\Omega} \nabla^2 B \, dV = 0,\tag{12}
$$

so that Laplacian terms do not contribute to mass conservation. Therefore, assuming $S_{\gamma}^{n+1} = 0$ and integrating equations (9) and (10), we get

$$
\int_{\Omega} A \, dV = \int_{\Omega} \gamma^* \, dV + \int_{\Omega} B \, dV \tag{13}
$$

$$
\int_{\Omega} \gamma^{n+1} \, dV = \int_{\Omega} A \, dV - \int_{\Omega} B \, dV \tag{14}
$$

$$
= \int_{\Omega} \gamma^* dV = \int_{\Omega} \gamma^n dV, \tag{15}
$$

¹⁰⁶ where the last equality comes from assuming conservative advection. Observe that the contents of *B* do not matter, ¹⁰⁷ since it is added before solving a Helmholtz equation and subtracted off afterwards. As a useful rule, terms that are ¹⁰⁸ not Laplacians must be added and subtracted in this way to achieve conservation.

Next we turn to the general form we want for our scheme. Schemes such as [36] also include $\nabla^2 F'(\gamma)$ terms, which we allow in our scheme as well. We also use γ^{AB} , described below, as an explicit estimate of γ^{n+1} . This leads to a potential general scheme of the form

$$
A + a_1 \nabla^2 A = \gamma^* + a_2 \gamma^{AB} + a_3 \nabla^2 F'(\gamma^{AB}) + a_4 F'(\gamma^{AB})
$$
\n(16)

$$
\gamma^{n+1} + c_1 \nabla^2 \gamma^{n+1} = A + c_2 \gamma^{AB} + c_3 \nabla^2 F'(\gamma^{AB}) + c_4 F'(\gamma^{AB}) + c_5 F'(\gamma^{n+1}),\tag{17}
$$

which adds in the necessary implicit treatment of F' but fails to be conservative since the $F'(\gamma^{n+1})$ term is not canceled (unless $c_5 = 0$, which would then not be implicit). To restore conservation, we need to cancel out the implicit term, which suggests a scheme of the form

$$
A + a_1 \nabla^2 A = \gamma^* + a_2 \gamma^{AB} + a_3 \nabla^2 F'(\gamma^{AB}) + a_4 F'(\gamma^{AB})
$$
\n(18)

$$
C + c_1 \nabla^2 C = A + c_2 \gamma^{AB} + c_3 \nabla^2 F'(\gamma^{AB}) + c_4 F'(\gamma^{AB}) + c_5 F'(\gamma^{n+1})
$$
\n(19)

$$
\gamma^{n+1} = C + g_2 \gamma^{AB} + g_3 \nabla^2 F'(\gamma^{AB}) + g_4 F'(\gamma^{AB}) + g_5 F'(\gamma^{n+1}), \tag{20}
$$

which will be conservative provided $a_2 + c_2 + g_2 = 0$, $a_4 + c_4 + g_4 = 0$, and $c_5 + g_5 = 0$. Schemes of this form exist, but the $F'(\gamma^{AB})$ terms are problematic, since $F(\gamma)$ has barriers at 0 and 1 but γ^{AB} need not lie within this range. Instead, we replace them with $F'(\gamma)^{AB} = 2F'(\gamma^n) - F'(\gamma^{n-1})$, which is safe to compute since $0 < \gamma^n < 1$ will always be bounded. This suggests we should look for a scheme of the form

$$
A + a_1 \nabla^2 A = \gamma^* + a_2 \gamma^{AB} + a_3 \nabla^2 F'(\gamma)^{AB} + a_4 F'(\gamma)^{AB}
$$
\n(21)

$$
C + c_1 \nabla^2 C = A + c_2 \gamma^{AB} + c_3 \nabla^2 F'(\gamma)^{AB} + c_4 F'(\gamma)^{AB} + c_5 F'(\gamma^{n+1})
$$
\n(22)

$$
\gamma^{n+1} = C + g_2 \gamma^{AB} + g_3 \nabla^2 F'(\gamma)^{AB} + g_4 F'(\gamma)^{AB} + g_5 F'(\gamma^{n+1})
$$
\n(23)

¹⁰⁹ subject to the constraints on the coefficients needed for conservation.

What remains is to select coefficients such that the scheme is consistent and formally 1.5 order accurate. We also prefer to discard terms from (23) where possible. Performing the truncation analysis leads to the scheme

$$
A - s\widehat{\Delta t}\nabla^2 A = \gamma^* - 2\gamma^{AB} + \widehat{\Delta t}M\lambda\nabla^2 F'(\gamma)^{AB}
$$
\n(24)

$$
C - s\widehat{\Delta t}\nabla^2 C = A + 2\gamma^{AB} - bs\widehat{\Delta t}^2 \nabla^2 F'(\gamma)^{AB} + b\widehat{\Delta t}F'(\gamma^{n+1})
$$
\n(25)

$$
\gamma^{n+1} = C - b\widehat{\Delta}t F'(\gamma^{n+1}),\tag{26}
$$

t¹¹⁰ where $s = \sqrt{\frac{M\lambda}{\hat{\Delta}t}}$ and $\hat{\Delta}t = \frac{2}{3}\Delta t$. This scheme is consistent for any constant *b*. We examine restrictions on this constant ¹¹¹ in Section 3.1.2. We show that the method is consistent and order 1.5 accurate in Section 3.1.3.

¹¹² *3.1.2. Avoiding nested solves*

113 We will solve (25) using Newton's method. Observe that for each Newton iteration, we must solve (26), which is a ¹¹⁴ pointwise nonlinear equation. To stabilize Newton's method, we would like to formulate it as an optimization problem ¹¹⁵ so that line searches can be employed. This requires us to integrate (25) with respect to *C* to form the objective, so that the optimality conditions recover (25). If we let $\gamma^{n+1} = f(C)$ denote the process of solving (26), then forming ¹¹⁷ the objective requires us to integrate the function f . If f is obtained as that output of a numerical procedure, then ¹¹⁸ computing this integral would be problematic. To have a practical chance of computing this integral, we will need a closed-form solution for *f*. Let *g* be the integral so that $\gamma^{n+1} = g'(C)$.

For most choices of the double-well potential F , the function $g'(C)$ will not be solvable in closed form. We must therefore restrict the form of F in such a way that it has the correct qualitative form while allowing g' to be computed and integrated in closed form. We note that this is possible for two special forms. If $F(x)$ is a cubic polynomial, then

$$
F(x) = a_3 x^3 + a_2 x^2 + a_1 x + a_0 \tag{27}
$$

$$
\gamma = C - b\widehat{\Delta t}F'(\gamma) = C - b\widehat{\Delta t}(3a_3\gamma^2 + 2a_2\gamma + a_1),\tag{28}
$$

which leads to a quadratic equation in γ that can be solved in closed form. Further, the quadratic equation for γ takes the general form $\gamma = g'(C) = k_0 +$ √ $k_1 + k_2C$, which can be integrated in closed form. Another form for *F* with this property is

$$
F(x) = a_2 x^2 + a_1 x + a_0 + a_3 \ln(x)
$$
 (29)

$$
\gamma = C - b\widehat{\Delta t}F'(\gamma) = C - b\widehat{\Delta t}(2a_2\gamma + a_1 + a_3\gamma^{-1}).
$$
\n(30)

Clearing the fractions leads to another quadratic equation in γ, this time of the form $\gamma = g'(C) = (k_0C + k_1) +$ $\sqrt{(k_0C+k_1)^2+k_2}$, which can also be integrated in closed form. (29) is notable in that it has a barrier at 0.

A suitable formulation of *F* must be a double-well energy function with barriers at 0 and 1. Neither form above has these properties, but a suitable function *F* can be constructed by combining energy terms of these forms piecewise. We note that piecewise formulations for *F* have been employed before [8, 28, 54]. It is clear that two logarithmic pieces will be required to get the necessary barriers. In addition, two cubic pieces are used to complete the double-well profile. We are thus looking for a potential of the form

$$
F(\gamma) = \begin{cases} F_0(\gamma) & 0 \le \gamma \le r \\ F_1(\gamma) & r < \gamma < \frac{1}{2} \\ F_1(1-\gamma) & \frac{1}{2} < \gamma \le 1-r \\ F_0(1-\gamma) & 1-r < \gamma \le 1 \end{cases} \tag{31}
$$

$$
F_0(\gamma) = b_2 x^2 + b_1 x + b_0 + b_3 \ln(x)
$$
\n(32)

$$
F_1(\gamma) = a_3 x^3 + a_2 x^2 + a_1 x + a_0 \tag{33}
$$

where we have assumed the symmetry $F(\gamma) = F(1 - \gamma)$.

When solving the equation $\gamma = C - b\widehat{\Delta t}F'(\gamma)$, there is an additional complication. The piecewise boundaries of ¹²⁴ $F'(\gamma)$ are in terms of γ, not *C*. The corresponding boundaries for *C* could of course be computed by substituting 125 boundary values for γ and solving for C, but we instead pursue a simpler strategy. We note that the double-well ¹²⁶ potential *F* will have two minima and a maximum. If we place the minima of *F* at *r* and 1 − *r* and the maximum at ¹²⁷ $\frac{1}{2}$, then $F'(r) = F'(\frac{1}{2}) = F'(1 - r) = 0$. If γ is one of these values, then $\gamma = C - b\widehat{\Delta t}F'(\gamma) = C$, so that the piecewise 128 boundaries for γ and *C* are the same.

The piecewise formulation for *F* has eight degrees of freedom. Enforcing *C* 2 continuity eliminates four degrees of freedom. Placing a minimum at *r* and shifting the minimum to zero (i.e., $F'(r) = F(r) = 0$) eliminates two more. We only need to construct $F(\gamma)$ up to a global scale (we will scale it appropriately later), which eliminates one more. We are left with one more degree of freedom, so we choose to enforce $C³$ continuity at *r*. We are now left with

$$
F_0(\gamma) = 3(\gamma - r)(8r^2 - 4ry - r + \gamma) - 12r^3 \ln \frac{\gamma}{r}
$$

$$
F_1(\gamma) = (r - \gamma)^2 (3 - 2r - 4\gamma).
$$
 (34)

Fig. 3: Plot of *F*(*C*) for different values of *r*: 0.1 ((1), 0.05 ((2), 0.02 ((2), 0.01 ((2), and 0.001 (2). The potential function converges pointwise in the limit $r \to 0$ over the range $0 < C < 1$.

Figure 2 shows a plot of $F(\gamma)$ and $F'(\gamma)$. Besides a global scale, this potential is also a function of the parameter ¹³⁰ *r*, which specifies the location of the minima. The dependence of this potential on *r* can be seen in Figure 3. The 131 potential converges in the limit $r \to 0$, which allows our scheme to be run with *r* very nearly zero. This is important, 132 since in regions far from the interface, γ will be comparable to *r* or $1 - r$.

The function $\gamma = g'(C)$ is defined as the solution of $\gamma = C - kF'(\gamma)$, where in the scheme we have the constant $k = b\hat{\Delta}t$. The global scaling on *F* is absorbed into the constant *b*. *g*' can be expressed in closed form as

$$
g'(C) = \begin{cases} g'_0(C) & 0 \le C \le r \\ g'_1(C) & r < C < \frac{1}{2} \\ 1 - g'_1(1 - C) & \frac{1}{2} < C \le 1 - r \\ 1 - g'_0(1 - C) & 1 - r < C \le 1 \end{cases}
$$
(35)

$$
q = 6k(1 - 2r) \qquad p = 1 + 6k(1 - 4r) \qquad s = 6r(1 - 6r)k \qquad (36)
$$

$$
g'_0(C) = \frac{1}{2p}h'_0(C+s) \qquad h'_0(x) = x + \sqrt{x^2 + L} = -\frac{L}{x - \sqrt{x^2 + L}} \qquad L = 48kr^3p \qquad (37)
$$

$$
g_1'(C) = \frac{1}{2} + h_1'\left(\frac{C - \frac{1}{2}}{12k}\right) \qquad h_1'(x) = K - \sqrt{K^2 - x} = \frac{x}{K + \sqrt{K^2 - x}} \qquad K = \frac{1 - q}{24k} \tag{38}
$$

We note that the first form of h'_0 and h'_1 is convenient for differentiation and integration, but the second form is more numerically robust since $x > 0$ and $K > 0$. In addition to $g'(C)$, which is used to compute γ^{n+1} , we also need *g* (for the optimization objective) and *g* ′′ (for the Hessian of the objective). The derivative *g* ′′ is straightforward

$$
g''(C) = \begin{cases} g''_0(C) & 0 \le C \le r \\ g''_1(C) & r < C < \frac{1}{2} \\ g''_1(1-C) & \frac{1}{2} < C \le 1-r \\ g''_0(1-C) & 1-r < C \le 1 \end{cases}
$$
(39)

$$
g_0''(C) = \frac{1}{2p}h_0''(C+s) \qquad h_0''(x) = 1 + \frac{x}{\sqrt{x^2 + L}} \qquad g_1''(C) = \frac{1}{12k}h_1''\left(\frac{C - \frac{1}{2}}{12k}\right) \qquad h_1''(x) = \frac{1}{2\sqrt{K^2 - x}} \tag{40}
$$

When computing the integral, we must be careful to ensure continuity.

$$
g(C) = \begin{cases} g_0(C) - g_0(r) + g_1(r) & 0 \le C \le r \\ g_1(C) & r < C < \frac{1}{2} \\ C - \frac{1}{2} + g_1(1 - C) & \frac{1}{2} < C \le 1 - r \\ C - \frac{1}{2} + g_0(1 - C) - g_0(r) + g_1(r) & 1 - r < C \le 1 \end{cases} \tag{41}
$$

$$
g_0(C) = \frac{1}{2p}h_0(C+s) \qquad h_0(x) = \frac{x}{2}h'_0(x) + \frac{L}{2}\ln\left(h'_0(x)\right) \tag{42}
$$

$$
g_1(C) = \frac{C}{2} + 12kh_1\left(\frac{C - \frac{1}{2}}{12k}\right) \qquad h_1(x) = Kx + \frac{2}{3}(K^2 - x)^{3/2} \tag{43}
$$

 $\frac{1}{33}$ In addition to *r*, the function *g'* also depends on *k*. The influence of this parameter is easier to understand in terms 134 of the related quantity *q*, as seen in Figure 4. In the limit $q \to 0$, $\gamma \to C$ when $0 < C < 1$, with γ clamped to 0 or 1 outside this interval. In the limit $q \to 1$, we have $g'(\frac{1}{2}) \to \infty$. For $q > 1$ the relationship $C = \gamma + kF'(\gamma)$ ceases to be 136 monotonic, so that its inverse g' does not exist as a continuous function. For the proposed scheme to exist, we must 137 have $0 < q < 1$. While *q* is always positive, the requirement $q < 1$ effectively imposes a time step restriction. Figure 5 shows plots of $g(C)$ and $g''(C)$. Note that $g''(C)$ is continuous and positive (from (39) and (40)), which improves the ¹³⁹ conditioning of the optimization problem.

¹⁴⁰ *3.1.3. Temporal discretization*

141 Our strategy for enforcing bounds on γ revolves around it ultimately being computed as $\gamma = g(C)$, where the 142 function $g(C)$ must be chosen to never produce a value outside the range $0 \le \gamma \le 1$. This requires our time integration ¹⁴³ scheme to take a very specific form. In Section 3.1.1, we motivated this general form and then selected a specific ¹⁴⁴ scheme of this form that satisfied all of our requirements. In Section 3.1.2, we constructed a potential energy function $F(y)$ that leads to a function $g(C)$ with suitable properties. With this, we have our completed scheme. In this section,

Fig. 4: Plot of *g* ′ (*C*) for different values of *q*: 0.99 (), 0.9 (), 0.5 (), 0.001 (). The function *g* ′ converges to piecewise-linear in the limit $q \to 0$ and develops an infinite slope at $C = \frac{1}{2}$ in the limit $q \to 1$. When $q > 1$, (26), when viewed as a function $C(\gamma)$, is not monotonic. In this case, *g'* would become multivalued. Useful values of *q* are thus restricted to $0 < q < 1$ to ensure that (26) has a unique and continuous of solution solution.

¹⁴⁶ we rederive our scheme algebraically in order to show that it is consistent and has formal convergence order 1.5. As ¹⁴⁷ with similar methods that are formally 1.5 order accurate, we observe second order convergence in our numerical tests ¹⁴⁸ [36, 27].

We begin by combining (1) and (2) to get the form of the Cahn-Hilliard equation that we wish to discretize:

$$
\frac{\partial \gamma}{\partial t} + \nabla \cdot (\mathbf{u}\gamma) = M\lambda \nabla^2 (F'(\gamma) - \nabla^2 \gamma) + S_{\gamma}.
$$
\n(44)

As in Goulding et al. [27], we discretize the time derivative using the second-order scheme $\frac{\alpha \gamma^{n+1}-\alpha \gamma^{BD}}{\Delta t}$ with $\alpha = \frac{3}{2}$ and $\frac{3}{7}$ $\frac{3}{7}$ ¹⁵⁰ $\gamma^{BD} = \frac{4}{3}\gamma^n - \frac{1}{3}\gamma^{n-1}$. For the first time step we use a first-order single-step scheme with $\alpha = 1$ and $\gamma^{BD} = \gamma^n$. Explicit quantities for **u** and γ are discretized using an Adams-Bashforth scheme, where $\gamma^{AB} = \gamma^n$, $\mathbf{u}^{AB} = \mathbf{u}^n$ in the first step ¹⁵² and $\gamma^{AB} = 2\gamma^n - \gamma^{n-1}$, $\mathbf{u}^{AB} = 2\mathbf{u}^n - \mathbf{u}^{n-1}$ in subsequent steps. We let $\widehat{\Delta t} = \Delta t/\alpha$, as α and Δt always occur together in ¹⁵³ practice.

Next, we derive the scheme presented in Section 3.1 directly from Equation (44). We begin with temporal discretization choices for γ and **u**,

$$
\frac{\gamma^{n+1} - \gamma^{BD}}{\widehat{\Delta t}} + \nabla \cdot \left(\mathbf{u}^{AB} \gamma^{AB} \right) = M \lambda \nabla^2 \left(F' \left(\gamma^{n+1} \right) - \nabla^2 \gamma^{n+1} \right) + S_{\gamma}^{n+1}.
$$
\n(45)

Next we split out the advection term as an update from γ^{BD} to an intermediate quantity γ^* :

$$
\frac{\gamma^* - \gamma^{BD}}{\widehat{\Delta t}} + \nabla \cdot \left(\mathbf{u}^{AB} \gamma^{AB} \right) = 0 \tag{46}
$$

$$
\frac{\gamma^{n+1} - \gamma^*}{\widehat{\Delta t}} = M\lambda \nabla^2 \left(F' \left(\gamma^{n+1} \right) - \nabla^2 \gamma^{n+1} \right) + S_{\gamma}^{n+1}.
$$
\n(47)

Expanding on Shen and Yang [51] and Goulding et al. [27], we define *s* so that $s^2\tilde{\Delta t} = M\lambda$ and introduce extra terms (denoted T_1 , T_2 , and T_3) to facilitate the further splitting of the equation. Each term introduces a small error but

Fig. 5: Plots of $g(C)$ (left) and $g''(C)$ (right) corresponding to $q = 0.5$ and $r = 0.1$.

decreases rapidly under refinement (noting $s = O(\Delta t^{-0.5})$ and $k = O(\Delta t)$, with *M* and λ fixed):

$$
T_1 = 2s(\gamma^{n+1} - \gamma^{AB}) = O(\Delta t^{1.5})
$$
\n(48)

$$
T_2 = -M\lambda k \nabla^2 \left(F'(\gamma^{n+1}) - F'(\gamma)^{AB} \right) = O(\Delta t^3)
$$
\n(49)

$$
T_3 = (ks - M\lambda) \left(F'(\gamma^{n+1}) - F'(\gamma)^{AB} \right) = O(\Delta t^2)
$$
\n⁽⁵⁰⁾

We incorporate the terms into Eq. (47) as

$$
\frac{\gamma^{n+1} - \gamma^*}{\widehat{\Delta t}} = \nabla^2 \left(M \lambda F'(\gamma^{n+1}) - M \lambda \nabla^2 \gamma^{n+1} + T_1 + T_2 + T_3 \right) + S_{\gamma}^{n+1}.
$$
\n(51)

Observe that the inclusion of T_1 formally limits us to convergence order 1.5. We define C according to (26) as

$$
C = \gamma^{n+1} + kF'(\gamma^{n+1}),
$$
\n(52)

Plugging in the definitions of T_1 , T_2 , T_3 , and C into Eq. (51), cancelling like terms, and rearranging, we get

$$
\frac{\gamma^{n+1} - \gamma^*}{\widehat{\Delta t}} = \nabla^2 \left(sC - s^2 \widehat{\Delta t} \nabla^2 C + (M\lambda - ks) F'(\gamma)^{AB} + s\gamma^{n+1} - 2s\gamma^{AB} + ks^2 \widehat{\Delta t} \nabla^2 F'(\gamma)^{AB} \right) + S_{\gamma}^{n+1}
$$
(53)

Using Eq. (52) to eliminate γ^{n+1} in Eq. (53) and defining

$$
A = C - s\widehat{\Delta t}\nabla^2 C - kF'(\gamma^{n+1}) - 2\gamma^{AB} + ks\widehat{\Delta t}\nabla^2 F'(\gamma)^{AB},\tag{54}
$$

Eq. (53) becomes

$$
A - s\widehat{\Delta t}\nabla^2 A = \gamma^* - 2\gamma^{AB} + \widehat{\Delta t}M\lambda\nabla^2 F'(\gamma)^{AB} + \widehat{\Delta t}S_{\gamma}^{n+1}.
$$
 (55)

Recall $\gamma^{n+1} = g'(C)$ as described in Section 3.1.2. Substituting this into Eq. (52) and rearranging, we get $kF'(\gamma^{n+1}) =$ $C - g'(C)$. Substituting this into Eq. (54) and combining the right hand side into *B*, we get a nonlinear equation satisfied by *C*:

$$
B = A + 2\gamma^{AB} - ks\widehat{\Delta t}\nabla^2 F'(\gamma)^{AB}
$$
\n
$$
g'(C) - s\widehat{\Delta t}\nabla^2 C = B.
$$
\n(56)

- ¹⁵⁴ From these expressions, we have our four-stage scheme:
- ¹⁵⁵ 1. Compute γ^* by advection using Eq. (46).
- ¹⁵⁶ 2. Solve the Helmholtz equation for *A* given in Eq. (55).
- ¹⁵⁷ 3. Solve the nonlinear equation for *C* given in Eq. (56).
- ¹⁵⁸ 4. Update γ^{*n*+1} as γ^{*n*+1} = *g'*(*C*).
- ¹⁵⁹ *3.1.4. Optimization-based formulation of the nonlinear solve*

We solve the nonlinear equation (56) for *C* by reformulating it as a minimization of the objective function

$$
E = \sum_{i} g\left(C_{i}\right) - \frac{1}{2} s \widehat{\Delta t} \sum_{i,j} C_{i} L_{ij} C_{j} - \sum_{i} C_{i} B_{i}, \tag{57}
$$

where *L* is the discrete Laplacian matrix. The corresponding gradient is

$$
\frac{\partial E}{\partial C_i} = g'(C_i) - s\widehat{\Delta t} \sum_j L_{ij} C_j - B_i
$$
\n(58)

so that the optimality conditions $\frac{\partial E}{\partial C_i} = 0$ reduce to (56). Since we will be using a Newton-based solver, we will also need the Hessian

$$
\frac{\partial^2 E}{\partial C_i \partial C_j} = \delta_{ij} g''(C_i) - s \widehat{\Delta t} L_{ij}.
$$
\n(59)

¹⁶⁰ Since $g''(C_i) > 0$, the Hessian is symmetric and positive definite. The optimization problem is thus convex, guar-¹⁶¹ anteeing a unique local minimum, which is also the global minimum. We solve this optimization problem using ¹⁶² Newton's method with Wolfe conditions line searches. We use zero as the initial guess during the first time step and C^{n-1} as the initial guess for the second time step. Thereafter, we warm-start our solver using $C^{AB} = 2C^{n-1} - C^{n-2}$ as ¹⁶⁴ the initial guess.

¹⁶⁵ *3.1.5. Boundary conditions*

We consider two types of boundary conditions for γ : periodic and Neumann ($\mathbf{n} \cdot \nabla \gamma^{n+1} = 0$). In order to solve both implicit equations, we need boundary conditions for *C* and *A*. From $\gamma^{n+1} = g'(C)$ we have

$$
\mathbf{n} \cdot \nabla \gamma^{n+1} = g''(C) \left(\mathbf{n} \cdot \nabla C \right). \tag{60}
$$

As $g''(C) \neq 0$, $\mathbf{n} \cdot \nabla \gamma^{n+1} = 0$ implies $\mathbf{n} \cdot \nabla C = 0$. For $\mathbf{n} \cdot \nabla A$, we start by substituting Eq. (52) into Eq. (54):

$$
A = C - s\widehat{\Delta t}\nabla^2 \gamma^{n+1} - ks\widehat{\Delta t}\nabla^2 F'(\gamma^{n+1}) - 2\gamma^{AB} + ks\widehat{\Delta t}\nabla^2 F'(\gamma)^{AB} - kF'(\gamma^{n+1})
$$
\n(61)

$$
= \gamma^{n+1} - 2\gamma^{AB} + s\widehat{\Delta t} \left(F'(\gamma^{n+1}) - \nabla^2 \gamma^{n+1} \right) - s\widehat{\Delta t} F'(\gamma^{n+1}) - k s \widehat{\Delta t} \nabla^2 \left(F'(\gamma^{n+1}) - F'(\gamma)^{AB} \right). \tag{62}
$$

As in [36], we define ξ^{n+1} to be a discrete version of the chemical potential following the derivation in Section 3.1.3 as

$$
\xi^{n+1} = \lambda \left(F'(\gamma^{n+1}) - \nabla^2 \gamma^{n+1} + \frac{2s}{M\lambda} \left(\gamma^{n+1} - \gamma^{AB} \right) - k \nabla^2 \left(F'(\gamma^{n+1}) - F'(\gamma)^{AB} \right) - \frac{(M\lambda - ks)}{M\lambda} \left(F'(\gamma^{n+1}) - F'(\gamma)^{AB} \right) \right). \tag{63}
$$

Substituting in our equation for *A* leads to

$$
A = \left(k - s\widehat{\Delta t}\right)F'(\gamma)^{AB} - \left(\gamma^{n+1} + kF'(\gamma^{n+1})\right) + \frac{s\Delta t}{\lambda}\xi^{n+1}.\tag{64}
$$

Recognizing that $\mathbf{n} \cdot \nabla F'(\gamma) = F''(\gamma) (\mathbf{n} \cdot \nabla \gamma)$, the boundary condition for *A* is

$$
\mathbf{n} \cdot \nabla A = \left(k - s\widehat{\Delta t}\right) \left(2F''(\gamma^n) \left(\mathbf{n} \cdot \nabla \gamma^n\right) - F''(\gamma^{n-1}) \left(\mathbf{n} \cdot \nabla \gamma^{n-1}\right)\right) - \mathbf{n} \cdot \nabla \gamma^{n+1} - kF''(\gamma^{n+1}) \left(\mathbf{n} \cdot \nabla \gamma^{n+1}\right) + \frac{s\Delta t}{\lambda} \mathbf{n} \cdot \nabla \xi^{n+1}
$$
\n(65)

$$
= \frac{s\Delta t}{\lambda} \mathbf{n} \cdot \nabla \xi^{n+1},\tag{66}
$$

¹⁶⁶ where we have used $\mathbf{n} \cdot \nabla \gamma^{n-1} = \mathbf{n} \cdot \nabla \gamma^{n} = \mathbf{n} \cdot \nabla \gamma^{n+1} = 0$. Following [36] we use the boundary condition $\mathbf{n} \cdot \nabla \xi^{n+1} = 0$, 167 which leads to $\mathbf{n} \cdot \nabla A = 0$. This gives us the necessary boundary conditions for both of our systems.

¹⁶⁸ *3.2. Navier-Stokes equations*

¹⁶⁹ *3.2.1. Temporal discretization*

We discretize the Navier-Stokes equations as in Goulding et al. [27]. As in Section 3.1.3, we discretize the time derivative as $\frac{\alpha \rho^{n+1} \mathbf{u}^{n+1} - \alpha(\rho \mathbf{u})^{BD}}{\Delta t}$ $\frac{A_1 - \alpha(\rho \mathbf{u})^D}{\Delta t}$. For the first time step, $\alpha = 1$ and $(\rho \mathbf{u})^{BD} = \rho^n \mathbf{u}^n$. To achieve second-order accuracy, we thereafter use a backwards-difference scheme with $\alpha = \frac{3}{2}$ and $(\rho \mathbf{u})^{BD} = \frac{4}{3}\rho^n \mathbf{u}^n - \frac{1}{3}\rho^{n-1} \mathbf{u}^{n-1}$. Explicit quantities for **u** are discretized using Adams-Bashforth, where $\mathbf{u}^{AB} = \mathbf{u}^n$ in the first time step and $\mathbf{u}^{AB} = 2\mathbf{u}^n - \mathbf{u}^{n-1}$ afterwards. As before, $\Delta t = \alpha \hat{\Delta t}$ is used to simplify the equations. \mathbf{u}^{ν} is an intermediate estimate of \mathbf{u}^{n+1} using an approximation for pressure, which is computed in an intermediate implicit solve, and m is the total density flux detailed in Section 3.2.2. With these, the discretized equations are

$$
\frac{\rho^{n+1}\mathbf{u}^* - (\rho\mathbf{u})^{BD}}{\widehat{\Delta t}} + \nabla \cdot \left(\mathbf{m} \otimes \mathbf{u}^{AB}\right) = 0\tag{67}
$$

$$
\frac{\mathbf{u}^{**} - \mathbf{u}^*}{\widehat{\Delta t}} = -\frac{1}{\rho^{n+1}} \nabla p^n + g + \frac{1}{\rho^{n+1}} \sigma \kappa \nabla \left(h \left(\gamma^{n+1} \right) \right) + \frac{1}{\rho^{n+1}} \nabla \cdot \left(\mu^{n+1} \left(\nabla \mathbf{u}^{AB} \right)^T \right) + \frac{1}{\rho^{n+1}} S_{\mathbf{u}}^{n+1}
$$
(68)

$$
\frac{\mathbf{u}^{\nu} - \mathbf{u}^{**}}{\widehat{\Delta t}} = \frac{1}{\rho^{n+1}} \nabla \cdot \left(\mu^{n+1} \nabla \mathbf{u}^{\nu} \right)
$$
(69)

$$
\nabla \cdot \left(\frac{1}{\rho^{n+1}} \nabla p'\right) = \frac{\nabla \cdot \mathbf{u}^{\nu}}{\widehat{\Delta t}}
$$
(70)

$$
\frac{\mathbf{u}^{n+1} - \mathbf{u}^{\nu}}{\widehat{\Delta t}} = -\frac{1}{\rho^{n+1}} \nabla p'.\tag{71}
$$

¹⁷⁰ *3.2.2. Momentum flux*

Everything in the Navier-Stokes equations is independent of Cahn-Hilliard except for the density flux term m. We follow Huang et al. [36] and Goulding et al. [27] and give a modification of m here that is consistent with our new Cahn-Hilliard discretization in Section 3.1.3. Beginning with

$$
\frac{\rho^{n+1} - \rho^{BD}}{\widehat{\Delta t}} + \nabla \cdot \mathbf{m} = S_m^{n+1},\tag{72}
$$

where **m** includes advection and Cahn-Hilliard separation, and S_m takes the effects of the forcing term S_γ , we express **m** in terms of γ :

$$
\nabla \cdot \mathbf{m} = -\frac{\rho^{n+1} - \rho^{BD}}{\widehat{\Delta t}} + S_m^{n+1}
$$
(73)

$$
= -(\rho_1 - \rho_0) \frac{\gamma^{n+1} - \gamma^{BD}}{\widehat{\Delta t}} + S_m^{n+1}
$$
 (74)

$$
= -(\rho_1 - \rho_0) \left(\frac{\gamma^{n+1} - \gamma^*}{\widehat{\Delta t}} + \frac{\gamma^* - \gamma^{BD}}{\widehat{\Delta t}} \right) + S_m^{n+1}.
$$
 (75)

Using Equations (46), (52), (54), and (55), defining $S_m^{n+1} = (\rho_1 - \rho_0) S_\gamma^{n+1}$, and canceling terms, this becomes γ

$$
\nabla \cdot \mathbf{m} = (\rho_1 - \rho_0) \left(\nabla \cdot \left(\mathbf{u}^{AB} \gamma^{AB} \right) - \nabla \cdot \left(s \nabla C + s \nabla A + (M\lambda - as) \nabla F'(\gamma)^{AB} \right) \right). \tag{76}
$$

As shown in [27], this definition of **is only well-defined up to a divergence-free shift. We determine the shift in** the same way as in that work, by considering the case $\rho_0 = \rho_1$. This leads to the same shift of $\nabla \cdot (\rho_0 \mathbf{u}^{AB})$ as in [27], which is consistent with the shift in [36]. We add this divergence-free shift to (76):

$$
\nabla \cdot \mathbf{m} = \nabla \cdot \left(\rho_0 \mathbf{u}^{AB} \right) + \left(\rho_1 - \rho_0 \right) \left(\nabla \cdot \left(\mathbf{u}^{AB} \gamma^{AB} \right) - \nabla \cdot \left(s \nabla C + s \nabla A + (M\lambda - as) \nabla F'(\gamma)^{AB} \right) \right). \tag{77}
$$

This leads to a definition of

$$
\mathbf{m} = \rho_0 \mathbf{u}^{AB} + (\rho_1 - \rho_0) \left(\mathbf{u}^{AB} \gamma^{AB} - s \nabla C - s \nabla A - (M\lambda - as) \nabla F'(\gamma)^{AB} \right). \tag{78}
$$

Like in [27], the term u *AB*γ ¹⁷¹ Like in [27], the term $\mathbf{u}^{AB}\gamma^{AB}$ is replaced by the flux computed by the WENO conservative advection described in ¹⁷² that work.

¹⁷³ *3.3. Discretization summary*

¹⁷⁴ For convenience, we provide a summary of a single step of the full discretized algorithm.

1. At the beginning of the step, the Adams-Bashforth and backwards-difference quantities must be computed from previous data. We compute γ^{BD} and γ^{AB} on cell centers and $(\rho \mathbf{u})^{BD}$ and \mathbf{u}^{AB} on cell faces. First-order time discretizations are used on the first time step:

$$
\gamma^{BD} = \gamma^n \qquad \gamma^{AB} = \gamma^n \qquad (\rho \mathbf{u})^{BD} = \rho^n \mathbf{u}^n \qquad \mathbf{u}^{AB} = \mathbf{u}^n \qquad \widehat{\Delta t} = \Delta t. \tag{79}
$$

Second-order time discretizations are used on every subsequence time step:

$$
\gamma^{BD} = \frac{4}{3}\gamma^n - \frac{1}{3}\gamma^{n-1} \qquad \gamma^{AB} = 2\gamma^n - \gamma^{n-1} \qquad (\rho \mathbf{u})^{BD} = \frac{4}{3}\rho^n \mathbf{u}^n - \frac{1}{3}\rho^{n-1} \mathbf{u}^{n-1} \qquad \mathbf{u}^{AB} = 2\mathbf{u}^n - \mathbf{u}^{n-1} \qquad \widehat{\Delta t} = \frac{2}{3}\Delta t. \tag{80}
$$

2. We use a conservative scheme as in [27] to compute γ^* from γ^{BD} as

$$
\gamma_{i,j}^* = \gamma_{i,j}^{BD} - \widehat{\Delta t} \left(\frac{\mathcal{F}_{i+1/2,j}^W - \mathcal{F}_{i-1/2,j}^W}{\Delta x} + \frac{\mathcal{F}_{i,j+1/2}^W - \mathcal{F}_{i,j-1/2}^W}{\Delta y} \right),\tag{81}
$$

where the fluxes \mathcal{F}^W are computed with WENO interpolation [39]. These fluxes are also stored for later use in 176 computing the mass flux **m**.

3. Next, we compute the intermediate term A from γ^* by solving the Helmholtz equation

$$
A - s\widehat{\Delta t}\nabla^2 A = \gamma^* - 2\gamma^{AB} + \widehat{\Delta t}M\lambda\nabla^2 F'(\gamma)^{AB} + \widehat{\Delta t}S_{\gamma}^{n+1}.
$$
\n(82)

4. We solve the nonlinear equation (56) for *C* by reformulating it as a minimization of the objective function

$$
E = \sum_{i} g(C_i) - \frac{1}{2} s \widehat{\Delta t} \sum_{i,j} C_i L_{ij} C_j - \sum_{i} C_i B_i.
$$
 (83)

5. The final phase fraction γ^{n+1} is computed from *C* using *g*['] (defined in (35)).

$$
\gamma^{n+1} = g'(C),\tag{84}
$$

6. With the Cahn Hilliard step complete, we begin the Navier-Stokes step. We compute effective densities and viscosities on faces by interpolating γ^{n+1} linearly to faces and then using equations (4) and (5).

$$
\rho_{i+\frac{1}{2},j}^{n+1} = \rho_0 + (\rho_1 - \rho_0) \gamma_{i+\frac{1}{2},j}^{n+1}
$$
\n(85)

$$
\mu_{i+\frac{1}{2},j}^{n+1} = \mu_0 + (\mu_1 - \mu_0) \gamma_{i+\frac{1}{2},j}^{n+1}.
$$
\n(86)

7. Compute the discrete mass flux using the Cahn-Hilliard intermediates *A* and *C*,

$$
\mathbf{m} = \rho_0 \mathbf{u}^{AB} + (\rho_1 - \rho_0) \left(\mathcal{F}^W - s \nabla C - s \nabla A - (M\lambda - as) \nabla F'(\gamma)^{AB} \right). \tag{87}
$$

8. Update momentum consistently with the movement of mass from Cahn-Hilliard as in [27]:

$$
\rho^{n+1} \mathbf{u}^* = (\rho \mathbf{u})^{BD} - \widehat{\Delta t} \nabla \cdot \left(\mathbf{m} \otimes \mathbf{u}^{AB} \right). \tag{88}
$$

- 9. Compute \mathbf{u}^* by dividing off ρ^{n+1} .
	- 10. Apply explicit forces:

$$
\mathbf{u}^{**} = \mathbf{u}^* + \widehat{\Delta t} \mathbf{g} + \frac{\widehat{\Delta t}}{\rho^{n+1}} \sigma \kappa \nabla \left(h \left(\gamma^{n+1} \right) \right) + \frac{\widehat{\Delta t}}{\rho^{n+1}} \nabla \cdot \left(\mu^{n+1} \left(\nabla \mathbf{u}^{AB} \right)^T \right) - \frac{\widehat{\Delta t}}{\rho^{n+1}} \nabla p^n + \widehat{\Delta t} S_{\mathbf{u}}^{n+1}
$$
(89)

Surface tension is descritized as in [27].

$$
\kappa = -\nabla \cdot \left(\frac{\nabla \gamma}{\|\nabla \gamma\|}\right) \tag{90}
$$

$$
h(\gamma) = \begin{cases} 1, & \text{if } \gamma \ge 1 - a \\ 0, & \text{if } \gamma < a \\ \frac{(-\gamma + a)^2 (2\gamma + 4a - 3)}{(2a - 1)^3}, & \text{otherwise} \end{cases}
$$
(91)

$$
a = 0.2
$$
 (92)

¹⁷⁸ The viscosity term is discretized consistently as in [36].

11. Solve the Helmholtz equation to apply the implicit portion of viscosity

$$
\mathbf{u}^{\nu} - \frac{\widehat{\Delta t}}{\rho^{n+1}} \nabla \cdot \left(\mu^{n+1} \nabla \mathbf{u}^{\nu} \right) = \mathbf{u}^{**}.
$$
 (93)

$$
\nabla \cdot \left(\frac{\widehat{\Delta t}}{\rho^{n+1}} \nabla p'\right) = \nabla \cdot \mathbf{u}^{\nu}
$$
\n(94)

$$
p^{n+1} = p^n + p',\tag{95}
$$

13. Project \mathbf{u}^{n+1} to be divergence free by applying the pressure correction:

$$
\mathbf{u}^{n+1} = \mathbf{u}^{\nu} - \frac{\widehat{\Delta t}}{\rho^{n+1}} \nabla p'.
$$
 (96)

¹⁷⁹ *3.4. Note on convergence order*

 The formal convergence order for our method based on Taylor series expansion is 1.5, yet we observe second order in our numerical tests. The leading truncation errors in our method are of orders 1.5 and 2, so that our error can be approximated as $\epsilon = A\Delta t^{1.5} + B\Delta t^2$. Here, the coefficient *A* gets the *T*₁ term, which is the sole source of errors at this order. By contrast, nearly all of the discretization errors in the method are second order and belong in *B*, including all of the spatial discretization errors as well as the backward difference and Adams-Bashforth temporal discretizations. In most schemes, the leading truncation terms are one order apart, such as $\epsilon = C\Delta t + D\Delta t^2 + O(\Delta t^3)$ or $\epsilon =$ $C\Delta t^2 + D\Delta t^3 + O(\Delta t^4)$. If at some low resolution (say 10) the *D* term contributed an error one order larger than the coefficient *C*, then around this resolution a convergence order of about 1.91 would be observed. If the resolution is increased one order of magnitude to resolution 100, the two error terms would contribute equally, and a numerical convergence order 1.50 would be observed. If the resolution is increased by another order of magnitude to resolution 1000, the numerical convergence order would be measured at 1.09, by which point the leading error term would be apparent.

Next, consider the current scheme, where the leading errors are of the form $\epsilon = A\Delta t^{1.5} + B\Delta t^2$. Under the same 193 conditions, where $B = 10A$ at resolution 10, a numerical convergence order of 1.95 is observed at this low resolution. ¹⁹⁴ By resolution 100, the order only drops to 1.88. By resolution 1000, the error is still only at 1.75. Only by resolution ¹⁹⁵ 16,000 does the observed convergence order drop as low as 1.6.

 The actual situation is of course far more complex than this simple example. For example, if the *A* and *B* terms ¹⁹⁷ have different signs, then the convergence orders in the above example at resolutions 10, 100, 1000, and 16000 are instead 2.05, 2.23, undefined, and 1.33. Given this analysis, it is not entirely surprising that second order convergence would be observed numerically for the proposed scheme.

²⁰⁰ 4. Numerical examples

²⁰¹ We demonstrate the numerical properties of our scheme through a series of numerical tests. All the units in the ²⁰² following tests are SI units.

		$r=0.1$	$r = 0.05$				$r = 0.01$					
N	\mathcal{L}_{2}	L_{∞}		\mathcal{L}_{2}		L_{∞}		\mathcal{L}_{2}		L_{∞}		
8	1.28e-05		2.12e-05		$1.28e-0.5$		$2.09e-0.5$		$1.27e-0.5$		$2.07e-0.5$	
16	$6.25e-06$	1.04	$1.27e-0.5$	0.74	$6.31e-06$	1.02	$1.27e-0.5$	0.72	$6.30e-06$	- 1.01	$1.27e-0.5$	0.70
32	3.84e-06	0.70	$1.22e-0.5$	0.05	3.85e-06	0.71	$1.22e-05$	0.05	3.85e-06	0.71	$1.23e-0.5$	0.05
64	$2.49e-06$	0.63	$1.14e-05$ 0.10		2.49e-06 0.62		$1.15e-0.5010$		2.50e-06	0.62	1.15e-05	0.09
128	8.64e-07	1.52	$4.85e-06$ 1.23		8.71e-07 1.52		$4.90e-06$ 1.23		8.76e-07	1.51	4.94e-06	1.22
256	1.85e-07	2.22	$1.05e-06$ 2.21		$1.86e-07$ 2.22		$1.05e-06$ 2.22		1.87e-07	2.22	$1.06e-06$	2.22
512	4.45e-08	2.05	2.55e-07	2.04	$4.48e-08$ 2.06		$\vert 2.57e-07 \vert 2.04 \vert$		$4.51e-08$	2.06	2.59e-07	2.04

Table 1: At larger *N*, our Cahn-Hilliard scheme shows second order convergence at *t* = 1.

²⁰³ *4.1. Manufactured solution*

We test our discrete solvers using a manufactured solution for γ , **u**, and *p*. Accuracy is measured by comparing the final simulated state against the manufactured solution. The source terms that enforce the manufactured solution are

$$
S_{\gamma} = \frac{\partial \gamma}{\partial t} + \nabla \cdot (\mathbf{u}\gamma) - \nabla \cdot (M\nabla \xi)
$$
\n(97)

$$
S_{\mathbf{u}} = \frac{\partial \rho \mathbf{u}}{\partial t} + \nabla \cdot (\mathbf{m} \otimes \mathbf{u}) + \nabla p - \rho g - \sigma \kappa \nabla (h(\gamma)) - \nabla \cdot \left(\mu \left(\nabla \mathbf{u} + (\nabla \mathbf{u})^T \right) \right). \tag{98}
$$

²⁰⁴ The accuracy of the Cahn-Hilliard solver is tested alone, then the Navier-Stokes solver is added for a second test ²⁰⁵ of the full system. We also perform two additional tests to show that changes in *r* and *b* do not affect the accuracy of ₂₀₆ our solver. The parameters used follow the similar tests in [36] and [27]. All tests use a $[-π, π]$ ² domain and end at 207 *t* = 1, with time step of $Δt = 0.08/N$ and cell size $Δx = 2π/N$. Fluid phase density is set to be $ρ_0 = 1$ and $ρ_1 = 3$ with viscosity constants $\mu_0 = 0.01$ and $\mu_1 = 0.02$. Unless otherwise noted, the Cahn-Hilliard parameters used in these tests 209 are $M = 0.001$, $\lambda = 0.001$, $\eta = 0.1$, $r = 0.1$, and $b = 0.01$.

²¹⁰ *4.1.1. Cahn-Hilliard solver*

To assess the convergence of the Cahn-Hilliard solver alone, we use the solution

$$
\gamma(x, y, t) = \frac{1}{2} + \frac{10}{21} \cos(x) \cos(y) (1 - \sin(t)).
$$
\n(99)

211 This solution is chosen such that $\mathbf{n} \cdot \nabla \gamma = 0$ and $\gamma \in (0, 1)$ within the time tested. We omit the Navier-Stokes update 212 for this test and set $u = v = 0$. The initial conditions are set using the manufactured solution for $t = 0$. We refine 213 *N* from 8 to 512 and use the L_2 and L_∞ errors at each level of refinement to measure the convergence rate. Table 1 ²¹⁴ shows that our Cahn-Hilliard solver exhibits second order convergence.

²¹⁵ *4.1.2. Cahn-Hilliard-Navier-Stokes solver*

In this test, we repeat the test in Section 4.1.1 with the same solution for γ but this time with the coupled Cahn-Hilliard-Navier-Stokes solver and non-zero solutions for *u*, *v*, and *p*:

$$
u(x, y, t) = \sin(x)\cos(y)\cos(t) \tag{100}
$$

$$
v(x, y, t) = -\cos(x)\sin(y)\cos(t)
$$
\n(101)

$$
p(x, y, t) = \cos(x)\cos(y)\sin(t),\tag{102}
$$

Table 2: The coupled Cahn-Hilliard-Navier-Stokes scheme shows second order convergence at *t* = 1.

							v u									
N	\mathcal{L}_{2} L_{∞}		$\sqrt{ }$		L_{∞}		₽		L_{∞}		L∩		L_{∞}			
8	1.77e-02		3.39e-02		5.52e-02		$1.35e-01$		$.74e-02$		$4.50e-02$		$2.03e-02$		$4.64e-02$	
16	2.98e-03	2.57	$9.28e-03$.87	1.23e-02	2.17	$3.18e-02$	2.08	$3.43e-03$	2.34	8.74e-03	2.36	$4.01e-03$	2.34	$.32e-02$	1.82
32	5.68e-04	2.39	$.42e-03$	2.71	$3.04e-03$	2.02	8.43e-03	1.92	7.64e-04	2.17	2.55e-03	. . 78	8.43e-04	2.25	2.48e-03	2.41
64	$.39e-04$	2.03	3.41e-04	2.06	7.59e-04	2.00	$2.14e-03$	1.97	.88e-04	2.02	6.24e-04	2.03	$2.10e-04$	2.01	6.40e-04	1.95
128	$3.49e - 0.5$	2.00	8.89e-05	L.94	1.91e-04	1.99	5.34e-04	2.01	4.81e-05	1.97	1.61e-04	.96	5.49e-05	.93	.60e-04	2.00
256	8.77e-06	99،	2.31e-05	1.94	4.82e-05	1.98	1.31e-04	2.02	.36e-05	1.83	4.40e-05	. 87	1.57e-05	80	4.68e-05	1.77

Table 3: L_2 and L_{∞} errors in γ for varying values of q.

q	h	Lρ	L_{∞}
$9.90e-01$	$1.32e+01$	$3.62e-0.5$	9.11e-05
9.00e-01	$1.20e+01$	3.60e-05	$9.05e-0.5$
8.00e-01	$1.07e+01$	3.57e-05	8.99e-05
7.00e-01	$9.33e+00$	3.54e-05	8.93e-05
$6.00e-01$	$8.00e+00$	3.52e-05	8.89e-05
5.00e-01	6.67e+00	3.51e-05	8.85e-05
$4.00e-01$	$5.33e+00$	$3.49e - 0.5$	8.84e-05
3.00e-01	$4.00e+00$	3.49e-05	8.83e-05
$2.00e-01$	$2.67e+00$	3.48e-05	8.84e-05
$1.00e-01$	$1.33e+00$	3.48e-05	8.86e-05
$1.00e-02$	1.33e-01	3.49e-05	8.89e-05
$1.00e-03$	1.33e-02	3.49e-05	8.89e-05
$1.00e-04$	1.33e-03	$3.49e-0.5$	8.89e-05
$1.00e-0.5$	1.33e-04	3.49e-05	8.89e-05
$1.00e-06$	1.33e-05	$3.49e-0.5$	8.89e-05

²¹⁶ which are the same solutions used in [36] and [27]. These solutions provide a divergence-free velocity field throughout ²¹⁷ the test. We set gravity to $g = \langle 1, -2 \rangle$. The manufactured solutions are used to set the initial and boundary conditions. 218 As in Section 4.1.1, *N* is refined from 8 to 256. The L_2 and L_∞ error is measured for γ , **u**, and *p* at each level of ²¹⁹ refinement and used to measure the convergence rate. Second order convergence is observed in all quantities as shown 220 in Table 2.

²²¹ *4.1.3. Varying b*

²²² Our time integration scheme includes one free parameter *b*. The convergence rate of the scheme is independent 223 of this parameter, though the parameter is bounded by the restriction $0 < q < 1$ as noted in Section 3.1.2. To evaluate 224 the effects of the constant *b* on the accuracy of the coupled Cahn-Hilliard and Navier-Stokes solvers, we fix $N = 128$ 225 and instead vary *b* (or equivalently, *q*). We use the same manufactured solutions as in the previous tests. Table 3 226 shows that the solver accuracy (represented by the L_2 and L_∞ error of γ) is insensitive to the choice of *b*. Although accuracy is not appreciably affected by b , we observe that the scheme is more stable when b is large. This is somewhat expected, since the strength of the barrier is proportional to *b*, as one observes in (25) and (26). Indeed, if $b = 0$, the 229 barrier is lost, and (25) reduces to a linear Helmholtz equation. Unless otherwise indicated, we run with $b = 0.01$ in 230 all of our numerical examples, except when this would result in $q > 0.5$; in this case, we compute *b* so that $q = 0.5$.

	(a) L_2 and L_{∞} error for γ_1 at varying r values.			(b) L_2 and L_{∞} error for γ_2 at varying r values.	
r	\mathcal{L}_2	L_{∞}	r	\mathcal{L}_2	L_{∞}
$4.00e-01$	3.48e-05	8.88e-05	$4.00e-01$	$1.33e-0.5$	3.54e-05
$3.00e-01$	$3.49e-0.5$	$8.89e-0.5$	$3.00e-01$	1.57e-05	$4.32e-0.5$
$2.00e-01$	$3.49e-0.5$	8.89e-05	$2.00e-01$	1.81e-05	5.18e-05
$1.00e-01$	$3.49e-0.5$	$8.89e-0.5$	$1.00e-01$	$2.05e-0.5$	$6.13e-0.5$
$1.00e-02$	$3.49e-0.5$	$8.89e-0.5$	$1.00e-02$	$2.28e-0.5$	7.08e-05
$1.00e-03$	$3.49e-0.5$	8.89e-05	$1.00e-03$	$2.30e-0.5$	7.18e-05
$1.00e-04$	$3.49e-0.5$	$8.89e-0.5$	$1.00e-04$	$2.31e-0.5$	$7.19e-05$
$1.00e-0.5$	$3.49e-0.5$	$8.89e-0.5$	$1.00e-0.5$	$2.31e-0.5$	$7.19e-05$
$1.00e-06$	$3.49e-0.5$	8.89e-05	$1.00e-06$	$2.31e-0.5$	$7.19e-05$

(a) L_2 and L_{∞} error for γ_1 at varying *r* values.

²³¹ *4.1.4. Varying r*

Our formulation of the potential F includes an extra free parameter r , which is the minimum of the double-well potential. In this test, we evaluate the effects of *r* on the accuracy of our solver. We test the coupled Cahn-Hilliard Navier-Stokes solver with two different manufactured solutions for γ over a range of values for *^r*. The first solution is the same as in the previous manufactured solution tests,

$$
\gamma_1(x, y, t) = \frac{1}{2} + \frac{10}{21} \cos(x) \cos(y) (1 - \sin(t)).
$$
\n(103)

This solution has $\gamma \in \left[\frac{1}{42}, 1 - \frac{1}{42}\right]$, which means that as *r* becomes very small the barrier portion of *F* outside the minima will never be used. To account for this, we repeat this test using the second manufactured solution

$$
\gamma_2(x, y, t) = \frac{1}{2}(1 - r)\left(1 + \cos\left(\frac{x}{2} + \frac{\pi}{2}\right)\cos\left(\frac{y}{2} + \frac{\pi}{2}\right)\right) + \frac{r}{2}.\tag{104}
$$

so that $\gamma \in \left[\frac{r}{2}, 1 - \frac{r}{2}\right]$ extends into the tails of *F*. The following solutions for **u** and *p* are used in both cases:

$$
u(x, y, t) = \sin(x)\cos(y)\cos(t) \tag{105}
$$

$$
v(x, y, t) = -\cos(x)\sin(y)\cos(t)
$$
 (106)

$$
p(x, y, t) = \cos(x)\cos(y)\sin(t). \tag{107}
$$

232 We fix $N = 128$ and vary r , as shown in Table 4. We observe that varying r does not strongly affect the accuracy, especially when *r* is small. This is consistent with the observation that *F* converges pointwise in the limit $r \to 0$, as ²³⁴ can be seen in Figure 3. The barrier portion of the *F* becomes extremely sharp in this limit. Unlike traditional barrier 235 methods, the sharpness of the barrier only weakly affects the performance of the method; although $F(\gamma)$ has a sharp $_{236}$ barrier in the limits γ → 0 and γ → 1, $F(g'(C))$ only grows gradually as *C* approaches infinity. We do sometimes 237 observe numerical difficulties when *r* is extremely small (below 10^{-4}). Unless otherwise specified, we run all of our $_{238}$ tests with $r = 0.01$.

²³⁹ *4.2. Binary separation of phases*

240 We demonstrate fluid phase separation over time using a random initial γ distribution. No forces are calculated $_{241}$ during this simulation and there is no γ source term. This test uses the same parameters as [27] and [32]. The domain

Fig. 6: Snapshots of phase separation over time.

²⁴² is $[0, 2\pi]^2$ with periodic boundaries. The initial distribution is uniformly random in the range $[0.475, 0.575]$. The time ²⁴³ step size is $\Delta t = 0.0001$ and the cell size is $\Delta x = 1/512$. The test runs until $t = 5$. The Cahn-Hilliard parameters are chosen to satisfy $ML = \eta^2 = 0.001$ with $\sigma = 1$. Figure 6 depicts the test results in several snapshots from $t = 0$ to $t = 5$. These snapshots are qualitatively similar to the results shown in [32], with increasing phase separation over ²⁴⁶ time.

²⁴⁷ *4.3. Stationary circle*

²⁴⁸ We test the balance between pressure and surface tension forces by simulating a stationary circle of fluid. We take ²⁴⁹ the test parameters from [36] and [27]. We measure the final velocity of the simulation to determine the magnitude ²⁵⁰ of the spurious currents caused by force imbalance. We test 5 cases with differing density ratios, surface tension, and ²⁵¹ viscosity, and show how each case changes under refinement.

252 We use a $[0, 1]^2$ domain with free-slip boundary conditions and cell size $\Delta x = 1/N$. The test runs until $t = 10$ ²⁵³ in time steps of $\Delta t = 0.064/N$. For each case we refine from $N = 16$ to $N = 256$. The circle of fluid is initialized 254 at $(0.5, 0.5)$ with radius $r = 0.2$ and density $\rho_1 = 1000$. The viscosity of the circle differs depending on test case. ²⁵⁵ The surrounding fluid varies in density and viscosity for each test case, and both fluids begin with no initial velocity. ²⁵⁶ Table 5 lists the density, viscosity, and surface tension parameters for each case.

Following [36] and [27], we narrow the interface width η with refinement to show convergence to a sharp interface solution:

$$
\eta = \eta_0 \left(\frac{\Delta x}{h_0}\right)^{X^{\eta}} = \eta_0 (Nh_0)^{-X^{\eta}}
$$
\n(108)

$$
M = M_0 \left(\frac{\eta}{\eta_0}\right)^{X^M} = \frac{M_0}{Nh_0}
$$
\n(109)

$$
\eta_0 = h_0 = \frac{1}{32} \qquad M_0 = 10^{-5} \qquad X^\eta = \frac{2}{3} \qquad X^M = \frac{3}{2}.\tag{110}
$$

257 As in [36] and [27], we average the final velocity to cell centers and compare the magnitude $||\mathbf{u}||_2$ with the ideal value ²⁵⁸ of 0. We compute the *L*² and *L*[∞] error and plot the change under refinement compared to the ideal first and second ²⁵⁹ order case in Figure 7. Figure 7b shows that *L*² decreases with first order whenever viscosity is nonzero, though no

Table 5: Material parameters for the five tested stationary circle cases.

Case ID	ρ_0	ρ_1	μ_0	μ_1	
Case 1	1000	1000	Ω	0	
Case 2	1000	1000	0.1	0.1	
Case 3		1000	0 ₁	0 ₁	
Case 4	1000	1000	0.0001	0.1	
Case 5	1000	1000	01	01	10

Fig. 7: The magnitude of the spurious velocity for the five stationary circle cases at different resolutions.

²⁶⁰ improvement is observed in *L*∞. That is, the maximum magnitude of velocity error does not change much, but the ²⁶¹ region over which this error occurs shrinks.

²⁶² We note that the test above is not a proper convergence test, since the coefficients of the PDE are changing under ²⁶³ refinement. As such, it is difficult to determine whether the problems observed are a consequence of the sharpening ²⁶⁴ interface or a fundamental problem with the underlying scheme. To determine whether the proposed method is ²⁶⁵ converging properly on this test, we hold the PDE fixed and perform a proper refinement study. We fix $\eta = 0.02$ and $M = 10^{-6}$. The results are shown in Figure 8, where we observe second order convergence in L_2 and convergence ²⁶⁷ ranging from first to second order in *L*∞.

 From these tests, we conclude that the method converges but is somewhat sensitive to the sharpness of the in- terface. We suspect that this is related to the smoothness of the Cahn-Hilliard potential. The potential function F is $C³$ continuous everywhere except at $\gamma = \frac{1}{2}$, where it is only $C²$ continuous. This suffices to produce a continuous Hessian. However, the time integration scheme includes terms of the general form $\nabla^2 F'(\gamma)$, which when expanded out depend on the third derivative of *F*. This may introduce small discontinuities in the numerical scheme near the interface, which surface tension is particularly sensitive to.

²⁷⁴ *4.4. Horizontal shear*

²⁷⁵ We examine conservation of mass, conservation of momentum, and change in kinetic energy in a shearing ad-²⁷⁶ vection test. Four cases with different density ratios and viscosities show the effects of these parameters on the test

Fig. 8: The magnitude of the spurious velocity for the five stationary circle cases with fixed interface width.

²⁷⁷ quantities. Surface tension and gravity are not used in this test.

The test setup is taken from [36] and [27]. The domain has periodic boundary conditions on all sides and has a range of $[0, 1]^2$. The time step size is $\Delta t = 0.0005$ and the tests run until $t = 1$. The cell size is $\Delta x = 1/128$. The surface tension constant is set to $\sigma = 10^{-12}$, leading to negligible surface tension forces, and $M = 10^{-7}$. The initial γ distribution is

$$
\gamma(x, y, 0) = \begin{cases} \frac{1}{2} \left(1 + \tanh\left(\frac{y - y_1}{\delta_1}\right) \right), & \text{if } y \le y_0 \\ \frac{1}{2} \left(1 + \tanh\left(\frac{y_2 - y}{\delta_1}\right) \right), & \text{if } y > y_0 \end{cases}
$$
(111)

$$
y_0 = 0.5
$$
 $y_1 = 0.25$ $y_2 = 0.75$ $\delta_1 = 1/30,$ (112)

with $\eta = \delta_1/$ √ 2. The shearing velocity is

$$
u(x, y, 0) = \begin{cases} \tanh\left(\frac{y - y_1}{\delta_1}\right), & \text{if } y \le y_0\\ \tanh\left(\frac{y_2 - y}{\delta_1}\right), & \text{if } y > y_0 \end{cases}
$$
(113)

$$
v(x, y, 0) = \delta_2 \sin(kx) \tag{114}
$$

$$
\delta_2 = 0.5 \qquad k = 2\pi. \tag{115}
$$

 These functions initialize fluid 1 with velocity in the postive *x* direction, located as a center band in the domain. Fluid 0 has a velocity in the negative *x* direction, and is located everywhere else. This distribution has a strong velocity gradient in the transition region between the fluids. Table 6 lists the variable parameters for the four different cases ²⁸¹ tested.

Following [27], we measured the change in total mass, total momentum, and kinetic energy using

$$
m_{\text{total}} = \sum_{i,j} \left(\rho_0 + (\rho_1 - \rho_0) \gamma_{i,j} \right) \Delta x^2
$$
 (116)

$$
(m\mathbf{u})_{\text{total}}^{x} = \sum_{i,j} \left(\rho_{i-1/2,j} \right) \left(u_{i-1/2,j} \right) \Delta x^{2}
$$
 (117)

$$
E_k = \frac{1}{2} \sum_{i,j} \left(\left(\rho_{i-1/2,j} \right) \left(u_{i-1/2,j} \right)^2 + \left(\rho_{i,j-1/2} \right) \left(v_{i,j-1/2} \right)^2 \right) \Delta x^2, \tag{118}
$$

Fig. 9: Example of Horizontal Shear (Case 3).

²⁸² with the y-axis momentum computed analogously to the x-axis. In the absence of surface tension and external forces, ²⁸³ kinetic energy should only decrease in the viscous cases 3 and 4, and otherwise remain unchanged. In all four cases, ²⁸⁴ momentum and mass should be conserved.

285 We plot the change in quantities ove time in Figure 10. In cases 1 and 3, where the fluids have matched densities, the density is constant throughout the domain and so mass is exactly conserved. In the other cases, there is a small change over time due to solver inaccuracies. Kinetic energy is conserved as expected in the inciscid cases 1 and 2, and declines due to viscosity in the remaining two cases. Momentum remains essentially unchanged in the *y*-axis, but we see a small negative trend over time in the *x*-axis. This change is on the order of our solver tolerances.

²⁹⁰ *4.5. Translating circle*

Based on the same test in [36] and [27], we test the accuracy of our coupled Cahn-Hilliard method with momentum advection. A drop of fluid 1 with radius 0.1 centered in the $[0, 1]^2$ domain is advected periodically with initial velocity 293 $\langle 1, 1 \rangle$ in the whole domain. We use cell size $\Delta x = 1/128$ and take time steps of $\Delta t = \Delta x/10$ until the simulation ends $_{294}$ at time $t = 1$. The drop is expected to complete one full revolution and return to its initial position. The Cahn-Hilliard parameters are set as $M = 10^{-7}$ and $\eta = 3\Delta x$. We test with different densities for the fluid 1, ranging from $\rho_1 = 1$ to $\rho_1 = 10^9$. Fluid 0 has density $\rho_0 = 1$ in all cases. The resulting large density ratios demonstrate the robustness of our ²⁹⁷ momentum conservation through advection. We do not test with viscosity or gravity. The tests are run twice, once 298 with the surface tension constant $\sigma = 10^{-12}$, giving negligible surface tension force, and the the second time with $299 \quad \sigma = 1$. The full set of cases are listed in Table 7.

Table 6: Material parameters for the four tested horizontal shear cases.

Case _{ID}	ρ_1	μ_0	μ_1
Case 1		\lq	
Case 2	10	$\mathbf{\Omega}$	0
Case 3		0.001	0.01
Case 4	10	0.001	O O1

Fig. 10: Conservation results for the four horizontal shear cases.

³⁰⁰ To evaluate the results of the test, we illustrate change in the velocity field as well as the shape of the drop. Ideally, 301 the velocity field does not change from its initial $(1, 1)$ values and the drop retains its circular shape. We measure the L_2 and L_∞ error in the velocity against its ideal values at the end of the simulation ($t = 1$). Figures 11 and Figure 12 303 depict the final state of the velocity field as staggered streamlines as well as the initial and final shape of the bubble. ³⁰⁴ These figures may be compared to those produced by Huang et al. [36] in a similar test. We see that in all cases the ³⁰⁵ numerical error is small enough that the velocity streamlines remain straight and the shape of the drop is preserved up ³⁰⁶ to density ratios of $\rho_1/\rho_0 = 10^9$, overlapping visually with the exact solution.

 Table 8 lists the measured error in the velocity field for the cases without surface tension. The velocity experiences negligible change at all density ratios. Table 9 lists the same measurements for the cases with surface tension. In this subset of cases, we see that there is more error in the velocity field, but this error decreases as the density ratio 310 increases. In all cases, the measured error is at least as small as the results reported in [36] and [27].

Case ID		ρ_1	
Case 1	1	1	-12
Case 2		10^{3}	10^{-12}
Case 3	1	10^{6}	10^{-12}
Case 4	1	10^{9}	10^{-12}
Case 5	1	1	1
Case 6	1	10^{3}	1
Case 7	1	10^{6}	1
Case 8		10^{9}	

Table 7: Material parameters for the eight translating circle cases.

Table 8: Velocity error for the four translating circle cases without surface tension (1–4).

Variable	Norm	$\rho_1/\rho_0 = 1$	$\rho_1/\rho_0 = 10^3$	$\rho_1/\rho_0 = 10^6$	$\rho_1/\rho_0 = 10^9$
u	\mathcal{L}_{2}	8.73e-13	2.70e-13	$2.92e-13$	2.89e-13
	L_{∞} L L_{∞}	7.33e-12	7.83e-13	8.76e-13	8.93e-13
		8.73e-13	$2.70e-13$	$2.92e-13$	2.89e-13
		7.33e-12	7.83e-13	8.76e-13	8.93e-13

Table 9: Velocity error for the four translating circle cases with surface tension (5–8).

³¹¹ *4.6. Rising air bubble*

312 We perform the rising air bubble test from [36] and [27] to examine how our scheme converges towards a sharp 313 interface solution. We test 6 different ways of coupling the interface width parameter η to the resolution *N* and 314 evaluate the results by measuring the circularity, center of mass, and rising velocity of a bubble surrounded by denser ³¹⁵ fluid.

316 We use a $[0, 1] \times [0, 2]$ domain with no-slip boundary conditions on the top and bottom edges and slip boundary ³¹⁷ conditions on the left and right edges. The cells are square with edge length [∆]*^x* ⁼ ¹/*N*. A circle of fluid 0 with 318 diameter 0.5, density $\rho_0 = 1$, and viscosity $\mu_0 = 0.1$ begins centered at position (0.5, 0.5). The surrounding fluid 1 319 has properties $\rho_1 = 1000$ and $\mu_1 = 10$. Gravity is set as $(0, -0.98)$, and $\sigma = 1.96$. The fluid begins at rest, and the 320 simulation runs until $t = 1$ with time step $\Delta t = 0.128/N$.

To couple η with *N* we use the following definitions from [36]:

$$
\eta = \eta_0 (Nh_0)^{-X_\eta} \tag{119}
$$

$$
M = M_0(\eta/\eta_0)^{X_M},\tag{120}
$$

where $\eta_0 = h_0 = 1/32$ and $M_0 = 10^{-7}$. X_η and X_M are varied over the 6 different test cases, and we limit them with $X_{\eta} \le 1$ based on [36] and $1 \le X_M < 2$ from [38]. Each of the 6 test cases is refined from $N = 16$ to $N = 256$. For 5 323 of the tests we test the effects of varying X_n by fixing $X_M = 1$ and varying X_n in the range [0, 1]. In the final test, we

Fig. 11: The initial state of the translating circle (Cases 1–4) is represented by the solid black line. The final $(t = 1)$ state is represented by the dashed red line. The blue dashed arrows represent the velocity streamlines at $t = 1$. We see that, as in the consistent momentum cases in [36], the streamlines appear straight and the drop shape is preserved up to a density ratio of $10⁹$.

324 increase *X_M* to 3/2 and use $X_\eta = 2/3$, which keeps *M* proportional to Δx .

Fig. 12: The initial state of the translating circle (Cases 5–8) is represented by the solid black line. The final (*t* = 1) state is represented by the dashed red line. The blue dashed arrows represent the velocity streamlines at $t = 1$. We see that, as in the consistent momentum cases in [36], the streamlines appear straight and the drop shape is preserved up to a density ratio of $10⁹$.

To measure the circularity (ψ_c), center of mass (y_c), and rising velocity (v_c), we use the methods from [36]:

$$
\psi_c = \frac{P_a}{P_b} = \frac{2\sqrt{\int_{\gamma < \frac{1}{2}} \pi d\Omega}}{P_b} \tag{121}
$$

$$
y_c = \frac{\int_{\Omega} y(1 - \gamma)d\Omega}{\int_{\Omega} (1 - \gamma)d\Omega}
$$
\n(122)

$$
v_c = \frac{\int_{\Omega} v(1 - \gamma)d\Omega}{\int_{\Omega} (1 - \gamma)d\Omega},
$$
\n(123)

Fig. 13: Results for rising air bubble case 1.

325 with P_a is the perimeter of a reference circle the same area as the bubble and P_b is the perimeter of the bubble itself. 326 Based on this ratio, when $\psi_c = 1$ the bubble is perfectly circular, and $\psi_c < 1$ will decrease as the bubble deforms. We compute P_b using the same method as [27].

³²⁸ We compare the measured values against the $N = 256$, using the L_2 error to measure the rate at which the test is 329 converging to a solution. Table 10 details the error and convergence rate for each case. Our results are comparable to those reported in [36] and [27]. In case 1, the interface width should not change with refinement, so the simulated 331 problem remains fixed at all N. We plot the change in our measured parameters over time for all refinements in Figure 13. We see in this figure that the parameters quickly converge to $N = 256$ values. Figure 14 demonstrates the 333 differences between the 6 cases at the highest level of refinement with $N = 256$. Our results for this test match the results shown in [36] and [27].

Fig. 14: Comparing results for all rising bubble test cases with $N = 256$.

³³⁵ *4.7. Rayleigh-Taylor instability*

³³⁶ The Rayleigh-Taylor instability experiment from [49] is a classic multi-phase fluid simulation. As in [36] and ³³⁷ [27], we reproduce this experiment with our scheme and measure key features over time.

338 The initial state positions a denser fluid with $\rho_1 = 3$ over a lighter fluid with $\rho_0 = 1$ in a [0, 1] × [0, 4] domain ³³⁹ discretized with cell size [∆]*^x* ⁼ ¹/128. The domain is periodic in the *^x*-axis and has free-slip boundary conditions at 340 the top and bottom walls. The interface between the fluids is set to an unstable pertubation at $y = 2 + 0.1 \cos(2\pi x)$, 341 which will allow immediate mixing. The only external force applied is a gravity of $(0, -1)$, and the fluids begin at 342 rest. The characteristic parameter $A_t = (\rho_1 - \rho_0)/(\rho_1 + \rho_0)$, the "Atwood ratio", is used to scale the time step of $\Delta t = 5 \times 10^{-4}$ / √ $\overline{A_t}$ and we run the simulation until *t* √ $\Delta t = 5 \times 10^{-4} / \sqrt{A_t}$ and we run the simulation until $t \sqrt{A_t} = 8$. Both fluids have matched viscosity $\mu_0 = \mu_1 = 0.001$, and we set the surface tension constant $\sigma = 10^{-12}$ and the Cahn-Hilliard parameters as $\eta = 0.01$ and $\lambda M = 10^{-15}$ 344 √ √

We show snapshots of this test in Figure 15 from *t* $\overline{A_t} = 0$ to *t* ³⁴⁵ We show snapshots of this test in Figure 15 from $t\sqrt{A_t} = 0$ to $t\sqrt{A_t} = 2.5$ for our scheme and provide a comparison with our implementation of [27]. Figure 16 shows the continuation of the test using our scheme from *t* √ ³⁴⁶ with our implementation of [27]. Figure 16 shows the continuation of the test using our scheme from $t\sqrt{A_t} = 2.25$

	Grid	$X_n = 0, X_M = 1$		$X_n =$	$\frac{1}{2}$, $X_M = 1$	$X_{\eta} =$	$\frac{1}{2}$, $X_M = 1$	$X_n = \frac{2}{3}$, $X_M = 1$		$X_{\eta} =$ $\frac{2}{3}$, $X_M = \frac{3}{2}$		$X_n = 1, X_M = 1$	
		\mathcal{L}_2		L_2		L_2		L_2		L_2		L_2	
ψ_c	16	4.91e-03		9.38e-03		1.14e-02		1.39e-02		1.38e-02		$2.00e-02$	
	32	1.61e-03	1.61	$2.30e-03$	2.03	2.78e-03	2.04	3.08e-03	2.17	$3.06e-03$	2.17	$3.22e-03$	2.64
	64	7.83e-04	1.04	8.71e-04	1.40	$7.92e-04$	2.04	$7.22e-04$	2.09	7.27e-04	2.08	8.61e-04	1.90
	128	$3.02e-04$	1.38	$3.32e-04$	1.39	$2.83e-04$	1.48	$3.51e-04$	1.04	3.66e-04	0.99	5.57e-04	0.63
		L_2 \mathcal{L}_{2}		L_2 \mathcal{L}_{2}		\mathcal{L}_{2}		\mathcal{L}_{2}					
	16	7.80e-03		1.38e-02		1.58e-02		1.79e-02		1.79e-02		2.33e-02	
y_c	32	2.01e-03	1.96	5.95e-03	1.21	$6.60e-03$	1.26	6.88e-03	1.38	6.87e-03	1.38	$6.96e-03$	1.74
	64	$4.53e-04$	2.15	$2.60e-03$	1.19	$2.63e-03$	1.26	$2.43e-03$	1.50	$2.42e-03$	1.50	1.88e-03	1.89
	128	9.74e-05	2.22	$9.51e-04$	1.45	8.64e-04	1.61	7.09e-04	1.78	7.01e-04	1.79	$4.25e-04$	2.14
		L_2		L_2		L_2		L_2		L_2		L_2	
	16	1.34e-02		1.98e-02		$2.20e-02$		$2.43e-02$		$2.43e-02$		3.05e-02	
v_c	32	4.48e-03	1.58	8.53e-03	1.21	$9.19e-03$	1.26	$9.40e-03$	1.37	9.38e-03	1.37	$9.42e-03$	1.69
	64	1.42e-03	1.66	$3.64e-03$	1.23	$3.64e-03$	1.26	3.34e-03	1.50	3.31e-03	1.50	$2.65e-03$	1.83
	128	$3.00e-04$	2.24	1.28e-03	1.50	$1.20e-03$	1.60	$9.91e-04$	1.75	9.70e-04	1.77	$6.42e-04$	2.04

Table 10: Rising air bubble test convergence results, using a comparison of simulations with *N* = 16 through *N* = 128 to corresponding simulations with $N = 256$.

to *t* √ 347 to $t\sqrt{A_t} = 8$. Our results are visually comparable to the snapshots shown in [36] and [27], and maintain symmetry 348 in the interface through the entire simulation. We also measure the location of the interface between the fluids from *t* √ $\overline{A_t} = 0$ to *t* √ $\tau \sqrt{A_t} = 0$ to $t \sqrt{A_t} = 2.5$, plotting the highest and lowest point of the interface in Figure 18. Our results are similar to ³⁵⁰ those of the experiments with similar parameters reported in [27], [36], [16] and [29]. As in these other works, the 351 simulation does not reach a stable state in the time given.

³⁵² As in [36] and [27], in Figure 17 we show a comparison of our scheme with different density values for fluid 1. We test densities $\rho_1 = 3, 30, 1000, 3000$, and our results for *t* √ $\overline{A_t} = 0$ to *t* √ ³⁵³ We test densities $\rho_1 = 3, 30, 1000, 3000$, and our results for $t\sqrt{A_t} = 0$ to $t\sqrt{A_t} = 1.75$ are similar to those shown in previous works. However, we note that our interface does not maintain symmetry past *t* √ ³⁵⁴ previous works. However, we note that our interface does not maintain symmetry past $t\sqrt{A_t} = 4$ for the larger density ratios at the given parameters. [36] and [27] do not report past *t* √ ³⁵⁵ ratios at the given parameters. [36] and [27] do not report past $t\sqrt{A_t} = 2$, so we cannot say whether this is a limitation ³⁵⁶ of this approach or just our scheme.

³⁵⁷ *4.8. Dam break*

³⁵⁸ We simulate a dam break scenario as described in Martin and Moyce [46], where a rectangular volume of water at ³⁵⁹ rest is released to flow in a larger container. This simulation shows how our scheme handles setups based on physical 360 phenonmenon. The initial square of water with side length $a = 0.05715$ is positioned in the lower-left corner of ³⁶¹ the [0, 4*a*] \times [0, 2*a*] domain. All walls in this domain are treated with the no-slip boundary condition, and each cell ³⁶² has size [∆]*^x* ⁼ *^a*/64. The initial velocity is zero everywhere in the domain. In our simulation, fluid 1 represents water with viscosity $\mu_1 = 1.002 \times 10^{-3}$ and density $\rho_1 = 998.207$. Fluid 2 represents air and has viscosity constant ³⁶⁴ $\mu_0 = 1.78 \times 10^{-5}$ and density $\rho_0 = 1.204$. The surface tension constant is $\sigma = 7.28 \times 10^{-2}$ and gravity of $\langle 0, -9.8 \rangle$ ³⁶⁵ is used as an external force. We set the Cahn-Hilliard parameters based on [36] and [27], which are $M\lambda = 10^{-7}$ and ³⁶⁶ $η = 0.01a$. We take time steps of $Δt = 7.1437 × 10^{-5}$ and run the simulation until $t = 10$.

367 As illustrated in Figures 20 and 21, when the simulation begins gravity causes the water to flow from the left edge ³⁶⁸ to the right edge of the domain. The water's momentum causes it to rise up the right wall of the domain, where gravity ³⁶⁹ overcomes the momentum and the water collapses back down on itself. Following [36] and [27], when reporting our

(b) Snapshots of a Rayleigh-Taylor simulation using our method.

results we non-dimensionalize *t* as $T = t \sqrt{\frac{|g_y|}{g}}$ ³⁷⁰ results we non-dimensionalize *t* as $T = t\sqrt{\frac{|g_y|}{a}}$ and length by dividing by *a*. Figure 19 shows the location of the front of the water *Z* and the highest point *H* from $T = 0$ to $T = 2.25$. These results compare well to the canonical experiment 372 results in Martin and Moyce [46] and the results reported in [36] and [27].

373 5. Conclusion

 In this paper we constructed a novel discretization of the Cahn-Hilliard equations that is able to guarantee that phase fractions remain bounded between 0 and 1. Maintaining phase fractions in the feasible range is essential for sta-376 bility, since values outside this range may produce negative densities, especially with large density ratios. The method 377 eliminates the need to perform a global post-processing step to correct the phase fraction. We constructed a formally 378 1.5 order accurate time integration scheme that uses a barrier potential to maintain bounds on the phase fraction. We 379 present a potential function that allows the barrier formulation to be cast as a convex nonlinear optimization problem, which can be solved efficiently and robustly. We coupled our Cahn-Hilliard solver to the Navier-Stokes equations 381 to simulate phase separation in a two-phase fluid flow in two dimensions. The resulting solver is mass-momentum 382 consistent and works with large density ratios. We demonstrate second order accuracy in γ and velocity and compare

Fig. 15: Visual comparison of Rayleigh-Taylor simulations using different methods at *^t* ⁼ ⁰, ¹, ¹.25, ¹.5, ¹.75, ², ².25, ².5.

Fig. 16: Continued snapshots of a Rayleigh-Taylor simulation using our method with $\rho_0 = 3$, from $t = 2.25$ to $t = 8$ in 0.25 increments.

it with published results on a number of tests.

 Since our method uses the same Navier-Stokes discretization and coupling as [27], we observe some of the same limitations, such as artifacts in the shearing test in Section 4.4. The method is sensitive to the sharpness of the 386 interface, likely related to the lack of C^3 continuity in the potential *F*; unfortunately, the current formulation does not ³⁸⁷ quite provide enough freedom to allow F to be C^3 everywhere. We have also observed that under some circumstances, the scheme suffers numerical difficulties or is not stable; this can occur when the parameters *r* or *b* are very small.

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Fig. 17: Snapshots of Rayleigh-Taylor simulations with different density ratios at *^t* ⁼ ⁰, ⁰.25, ⁰.5, ⁰.75, ¹, ¹.25, ¹.5, ¹.75.

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Fig. 18: Tracking the maximum and minimum *y* of the phase interface in the Rayleigh-Taylor simulation with $\rho_1/\rho_0 = 3$.

(a) The largest *x* location of fluid phase 1 over time.

(b) The largest *y* location of fluid phase 1 over time.

Fig. 19: Tracking the height and front of fluid phase 1 in the dam break scenario.

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Fig. 20: Snapshots of the dam break scenario from $T = 0$ to $T = 4.5$.

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Fig. 21: Snapshots of the dam break scenario from $T = 5$ to $T = 9.5$.

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